

24 extracts. Among the valuable volatile compounds, the most abundant are linoleic (31.11-
25 41.47%) and hexadecanoic (15.22-20.58%) acid, osthol (4.53-5.42%), and 7-methoxy-8-(2-
26 oxo-3-methylbutyl) coumarin (12.65-15.45%). Extracts obtained by UAE were analyzed by
27 HPLC, where the dominant compounds were identified as hesperidin (848-900.24 [$\mu\text{g/ml}$]),
28 narirutin (16.70-18.16 [$\mu\text{g/ml}$]), naringin (771.45 -830.39 [$\mu\text{g/ml}$]) and rutin (47.53-104.40
29 [$\mu\text{g/ml}$]). Finally, the *in silico* testing was performed to identify pharmacologically the most
30 valuable bioactive compounds in the extracts, and to enable screening of the possible
31 pharmacological effect and applications of the obtained.

32 **Keywords:** Orange peel; Herbal dust; Supercritical extraction; Ultrasound-assisted extraction;
33 Polyphenols; *In silico* evaluation

34

35 **1. Introduction**

36 Citrus fruits are the most produced and consumed fruits in the world, both in fresh form and
37 as a juice (Murador et al., 2019). According to the data of the Food and Agriculture
38 Organization of the United Nations (FAO, 2021), it is estimated that 143,755.6 thousand tons
39 of citrus were produced in 2019, of which 76,292.6 thousand tons were oranges. Because of a
40 large world production and processing, large quantities of various citrus by-products and
41 wastes are formed. This represents a huge problem in the waste disposal means, as well as a
42 large economic burden for the citrus processing sectors. In the case of citrus, according to
43 Mahato et al. (2018), the edible parts of citrus are pulp and juice, while segment walls, peel,
44 pith residues and seeds are not edible and represent citrus waste (CW). The amount of CW
45 ranges between 50-60% of processed fruit and depends on several factors such as the juice
46 extraction system, citrus varieties, and the amount of water for processing (Taghizadeh-
47 Alisaraei et al., 2017). Sharma et al. (2019) defined the composition of CW as follows: 40-
48 55% of peel, 30-35% of internal tissues and less than 10% of seeds. The orange peel, as one
49 of the dominant CWs, contains a large amount of high value-added compounds such as
50 polyphenols, carotenoids, dietary fibre, sugars, essential oils, ascorbic acid, and significant
51 amounts of certain trace elements (zinc, magnesium, etc.) (Osarumwense et al., 2013; Putnik
52 et al., 2017).

53 Essential oil (EO) and polyphenolics of the orange peel are the most important health
54 beneficial constituents of this raw material. The unique orange peel EO aroma is formed due
55 to the presence of terpene hydrocarbons, ketones, aldehydes, esters, and alcohols (Qiao et al.,
56 2008). Limonene is mentioned as the main component of this EO, however, other components
57 such as linalool, octanal, citronellal, geranial and α -terpineol are present too, but in the lower
58 concentrations (Gonçalves et al., 2018). The application of this kind of EO, as well as of
59 individual volatiles of the EO, is significant in the production of pharmaceutical products,

60 food flavour additives, natural antimicrobials (Bakkali et al., 2008), in production of cleaning
61 products, and in the perfume industry (Sharma et al., 2017). Flavonoids and phenolic acids are
62 the most important polyphenolics of orange peel (Feng, 2022). Hesperidin can be isolated as
63 the most common flavonoid in every part of citrus, as well as in the peel (Huang & Ho, 2010).
64 Hesperidin has a number of different properties, such as a positive effect on the vascular or
65 cardiovascular system (Morand et al., 2011), protective effect in case of radiation exposure
66 (Hosseinimehr et al., 2009; Kalpana et al., 2009), anticancer activity (Aggarwal et al., 2020),
67 antimicrobial activity (Corciova et al., 2015), anti-inflammatory and antioxidant activity
68 (Tejada et al., 2018). In addition to hesperidin, naringin is another important flavonoid present
69 in citrus fruits. Several studies have shown that naringin supplementation is useful in the
70 treatment of obesity, hypertension, diabetes, and metabolic syndrome (Alam et al., 2014).

71 Bioactive compounds from waste and by-products, such as orange peel, can be extracted
72 using traditional extraction techniques (Haya et al., 2019). However, due to the insufficient
73 efficiency and cost-effectiveness of these methods, long extraction time, thermal degradation
74 of thermolabile active compounds, as well as frequent use of toxic, organic solvents (hexane,
75 petroleum ether, etc.) (Putnik et al., 2017), there is an increasing tendency for the application
76 of modern green extraction techniques in order to overcome such limitations (Vidović et al.,
77 2021a). The choice of the most adequate technique, as well as the set-up of working
78 conditions, significantly affects the chemical composition of the extracts obtained and their
79 biological activity. According to the literature data, supercritical carbon dioxide extraction
80 (Sc-CO₂) is an excellent technique for the isolation of citrus peel EO, while for the isolation
81 of peel polar components, ultrasound-assisted extraction (UAE) can be selected (Jokić et al.,
82 2020). Extraction technology based on the use of CO₂ in the supercritical state is widely
83 recognized as safe and has been used as a green approach for productive extraction and
84 recovery of valuable compounds from various raw materials (Vidović et al., 2021). CO₂ has

85 many advantages over organic solvents, while its selectivity, as well as density and other
86 physico-chemical properties, can be adjusted by the change of process temperature and
87 pressure (or both) (Aiello et al., 2020). As extracts obtained by Sc-CO₂ are free of applied
88 extraction solvent, the production of the extract without need for additional purification can
89 be highlighted as another important aspect of this technique. UAE can be performed using an
90 ultrasound bath or ultrasound probe, which are based on a piezoelectric transducer as a source
91 of ultrasound power. UAE, in addition to being relatively cheap, has many advantages over
92 conventional methods, some of which are less time and energy, low temperature extraction
93 and maintaining the quality of the extract (Kumar et al., 2021). According to the studies, UAE
94 gives higher contents of total phenols and flavonoids compared to conventional solvent
95 extractions due to the cavitation and destruction of the cell walls, which occur during the
96 propagation of ultrasound waves through the solvent. Consequently, there is an increase in the
97 mass transfer and release of compounds from the material (Živković et al., 2022). For both
98 extraction methods the important fact is that they are already recognized by the industry and
99 are scalable on the industrial level.

100 Considering all, the study has targeted the orange peel dust (OPD) as the waste material of
101 interest which was generated in the filter tea factory. Namely, during industrial processing of
102 dried orange peel a large amount of powder (even up to 35%) accumulates with a particle
103 diameter <0.315 mm, which is less than the pore size of filter paper; therefore, this kind of
104 material is impossible to be used in the further production (Vidović et al., 2021). This residual
105 fraction represents a raw material still containing a wide range of bioactive compounds which
106 can be isolated and potentially value-added products can be obtained. As novel studies are
107 showing, the integration of different extraction processes represents an attractive approach to
108 the production of different valuable products from the same raw material, where both non-
109 polar and polar fractions can be isolated (Osorio-Tobón, 2020). Besides, according to the

110 results of Dias et al. study (2019) the integrated process (Sc-CO₂ and UAE) can increase the
111 UAE efficiency. Therefore, this approach has been applied in the case of OPD processing and
112 utilisation. To the best of knowledge, this is the first report focused on the application of
113 integrated, green-based extraction technologies (Sc-CO₂ + UAE) for the recovery of high-
114 value compounds from this kind of material.

115 **2. Material and Methods**

116 **2.1. Plant material and chemicals**

117 The orange peel (*Citrus sinensis* L.) dust (OPD) was obtained from the local filter tea factory
118 Fructus d.o.o. (Bačka Palanka, Serbia). It represents the material in the form of powder with
119 particle size <0.315 µm. The moisture content of the raw material was 3.36 ± 0.63%.

120 For Sc-CO₂, commercial CO₂ (purity 99.9%, v/v) was used (Messer, Novi Sad, Serbia). All
121 other chemicals used during the experiment were analytical purity reagents. For HPLC,
122 mobile phases (methanol and acetic acid) were obtained from J.T. Baker (Phillipsburg, NY,
123 USA) where methanol was HPLC grade, while acetic acid was an analytical grade. The
124 ultrapure water (conductivity ≤ 0.054 µS/cm) used for the preparation of the mobile phase
125 was obtained from a Milli-Q water purification system Simplicity 185 by Millipore (Bedford,
126 MA, USA). The standard of rutin (purity 97%) was purchased from Acros Organics (Geel,
127 Belgium), the standard of hesperidin (purity 89.5%) was obtained from Dr Ehrenstorfer
128 GmbH (Augsburg, Germany), while narirutin (purity 98%) and naringin (purity 95%), were
129 purchased from Sigma-Aldrich (Steinheim, Germany).

130 **2.2. Sc-CO₂ extraction**

131 The high-pressure extraction was carried out using a high-pressure extraction system (HPEP,
132 NOVA-Swiss, Effretikon, Switzerland) with Sc-CO₂ as the extraction solvent. The Sc-CO₂

133 extraction of OPD was conducted at pressures 100, 200 and 300 bar at temperature 40 °C
134 using 30 g of the plant material. The extraction kinetics were monitored in the time intervals
135 of 0.5, 1, 1.5, 2, 3 and 4 h. During extraction, the pressure and temperature in the separator
136 unit were 15 bar and 23 °C, while the flow rate was set at 1.94 kg/h. Using this extraction
137 procedure 3 different supercritical OPD extracts were prepared.

138 **2.3. Ultrasound-assisted extraction**

139 UAE was provided for 3 different materials left after extraction by Sc-CO₂. These are:
140 material left after extraction by Sc-CO₂ at 100 bar, marked as SFE-100, material left after
141 extraction by Sc-CO₂ at 200 bar, marked as SFE-200, and material left after extraction by Sc-
142 CO₂ at 300 bar, marked as SFE-300. Each material was extracted by 50% ethanol/water
143 solution (v/v) in a solid liquid ratio of 1:20 (w/v) using a sonotrode (UP400St ultrasonic
144 processor, Hielscher, Germany) with varying amplitude (20, 60 and 100%) and at the
145 temperature up to 50 °C. Thus, from each material left after Sc-CO₂ extraction three different
146 liquid OPD extracts were prepared. The extraction time was limited by reaching the set
147 temperature. Energy consumption, as well as the increase and change of the process
148 temperature itself were recorded. Beside of this, using the same procedure extraction of
149 untreated raw material (OPD which was not previously extracted by Sc-CO₂) was performed
150 in order to evaluate efficiency of the process integration-coupling of two green methods (Sc-
151 CO₂ extraction followed by UAE). After extraction, obtained extracts were stored in the
152 refrigerator until the analysis.

153 **2.4. Determination of total phenols and total flavonoids in OPD liquid extracts obtained** 154 **by UAE**

155 The content of total phenols (TPC) in extracts was determined by the Folin-Ciocalteu method
156 (Singleton et al., 1999). At a wavelength of 750 nm, the absorbance was measured using a
157 UV/VIS single-beam spectrophotometer (6300 Spectrophotometer, Jenvai, UK). The results

158 are expressed as gallic acid equivalent (GAE) per gram of dry weight (mg GAE/g dw). All
159 experiments were performed in triplicate, and the results were expressed as mean values.

160 The content of total flavonoids (TFC) was determined by colorimetric analysis of aluminium
161 chloride (Harborne, 1989). The results obtained are expressed as mg of catechin equivalent
162 (CE) per gram of dry weight (mg CE/g dw). All experiments were performed in triplicate, and
163 the results were expressed as mean values.

164 **2.5. GC-MS analysis of supercritical OPD extracts**

165 For the analysis of supercritical OPD extracts obtained in the first process step- SC-CO₂, a gas
166 chromatograph and mass spectrometer instrument model 7890A (Agilent Technologies, Palo
167 Alto, CA, USA) with 5975C mass detector (Agilent Technologies, Palo Alto, CA, USA) was
168 used. The capillary column was HP-5 MS (30 m, 0.25 mm, 0.25 μm). As the carrier gas
169 helium was used with a flow rate of 1 mL/min. The conditions for the analysis were: the
170 injector temperature of 250 °C (split ratio 1:50), and the temperature regime was isothermal at
171 70 °C for 2 min and then, increased from 70 °C to 200 °C at 3 °C/min. The parameters for the
172 MS detector were: ionisation energy of 70 eV, ion source temperature 230 °C, and scanning
173 range of 45-450 *m/z*. The extracts obtained with Sc-CO₂ (10 mg) were diluted with hexane
174 and 1 μL of the solution was inserted into the GC injector. Identification of the compounds
175 was performed by the comparison of their retention indices (RI), determined relative to the
176 retention times of *n*-alkanes (C₉-C₂₅), and qualitative identifications of present compounds
177 were performed using Wiley 9 (Wiley, New York, NY, USA) and NIST 17 (D-Gaithersburg)
178 databases. Percentage of the compound's composition was calculated from the GC peak areas
179 using the normalisation method without correction factors. The average components values
180 were calculated from duplicate GC-MS analyses of all extracts (Šafranko, 2021).

181 **2.6. HPLC analysis of liquid OPD extracts obtained by UAE**

182 Determination of polyphenols was performed by HPLC (high performance liquid
183 chromatography) method, on Cosmosil 5C18-MS-II column (Nacalai Tesque, Inc., Kyoto,
184 Japan), 250 mm long with an internal diameter of 4.6 mm, filled with 5 μm particles. The
185 analysis was performed on a semi-preparative HPLC device (Agilent, 1260 Infinity II series).
186 The HPLC system used for the analysis consisted of a quaternary pump (G7111A), a column
187 chamber (G7116A), a photo-diode array detector (G7115A), an autosampler (G7157A), and a
188 fraction collector (G1364E). The system was operated using a computer program Prep LC
189 Online. The separation of analysed compounds was performed by gradient elution for 50 min,
190 where 1% CH_3COOH (in Milli-Q water) was used as the phase A and methanol as the phase
191 B, with 80:20 ratio of A:B. The flow rate was 1.0 mL min^{-1} , the injection volume was $20 \mu\text{L}$,
192 the UV detection wavelength was 283 nm, and the analysis was performed at $25 \text{ }^\circ\text{C}$. The
193 gradient conditions were: 0-5 min 80% of A, 5-15 min 80-40% of A, 15-35 min holding 20%
194 of A, 35-40 min 20-40% of A, 40-50 min 40-80% of A. The standard stock solution for
195 hesperidin was prepared in dimethyl sulfoxide (DMSO) and diluted with methanol. The
196 calibration for hesperidin was obtained at seven concentrations (1.0-1500 mg/L). The linearity
197 of the calibration curve was confirmed by $R^2 = 0.99920$ for hesperidin. The retention time for
198 hesperidin was 18.838 min (Šafranko, 2021).

199 **2.7. *In silico* studies**

200 The target prediction for a selected set of small molecules was carried out using
201 pharmacophore approach implemented in Phrammapper, a reverse docking server (Liu et al.,
202 2010). For each molecule, three-dimensional structures stored in a.mol2 format were
203 submitted to generate a list of 300 potential proteins from the database of all targets
204 containing 7302 entries (v2010). All other parameters were kept at their default values.

205 The docking of selected components identified in the citrus extracts against liver
206 carboxylesterase 1 (PDB ID: 2DR0) was conducted using AutoDock Vina (ver. 1.1.2) (Trott
207 & Olson, 2010) within the VegaZZ scripting environment (ver 3.2.2.21). The library of the
208 natural products was built by converting SMILES strings into mol2 files using OpenBabel
209 (ver. 2.4.1) (Pedretti et al., 2021). The protein target was prepared by removing water
210 molecules and adding hydrogens atoms. The co-crystallized ligand in the binding site was
211 removed from structures prior to docking and its centre of mass was used to position a box
212 with the sizes of 24 Å x 24 Å x 24 Å. Generally, the docking settings were kept to its default
213 values except exhaustiveness that was set to 50, and the top five favourable binding poses
214 were saved for each molecule.

215 Molecular properties of selected components were predicted using DataWarrior software
216 (Sander et al., 2015) and SwissADME web server (Daina et al., 2017).

217 **3. Results and Discussion**

218 **3.1. Sc-CO₂ extraction of OPD**

219 By integrating two advanced green extraction techniques, Sc-CO₂ extraction and UAE, the
220 more efficient reuse of citrus by-products and wastes could be achieved, and a higher number
221 of valuable compounds and products could be obtained. Side to this, according to Jokić et al.
222 (2020) the advantage of using Sc-CO₂ extraction is not only related to better oil yield, but also
223 to the reduction of artefacts created by conventional methods. The application of Sc-CO₂
224 extraction enables isolation of aromatic and volatile compounds from citrus waste, as well as
225 fatty acids, certain pigments, and waxes, while in exhausted material left after Sc-CO₂
226 extraction, polar constituents, such as bioflavonoids, stayed unused. This material therefore
227 could be further processed for the isolation of polar compounds, using techniques such as
228 UAE, making the whole process of citrus peel utilisation much more efficient.

229 Obtaining non-polar compounds of different complexity can be achieved by varying the
 230 operating pressures during Sc-CO₂ extraction (Jokić et al., 2020). Pressure is the most
 231 dominant process parameter in Sc-CO₂ extraction, and its variation is making a large
 232 difference in general extraction yield and extract quality. Therefore, in order to find out the
 233 best process set-up for the extraction of non-polar compounds from the targeted material
 234 OPD, the efficiency of Sc-CO₂ extraction in dependence to working pressure (100, 200 and
 235 300 bar) was analysed, while the process temperature and the CO₂ flow were kept as constant.

236 According to the results, Sc-CO₂ extraction of OPD provided, for a total extraction time of 4
 237 h, very similar yields in the range of 0.61-0.64%. The highest yield Sc-CO₂ extraction was
 238 achieved at 300 bar. Barrales et al. (2018), in the study on supercritical extraction of orange
 239 peel, obtained a total extraction yield of $0.48 \pm 0.02\%$ at a pressure of 350 bar and a
 240 temperature of 40 °C, which is less compared to our study. On the other hand, Benelli et al.
 241 (2010) at the temperature of 40 °C and a pressure of 300 bar achieved the yield of $1.37 \pm$
 242 0.09% in the total extraction time of 5 h. The difference between the extraction yields is
 243 impacted by the raw material drying process, quality and characteristics (particle size and
 244 shape), the orange variety, and this may explain variation in the total extraction yield in the
 245 literature data.

246 Supercritical OPD extracts obtained at different process pressures were analysed by GC-MS.
 247 The obtained volatile profile of extracts is shown in Table 1.

248 Table 1. Volatile profile of supercritical OPD extracts.

No.	Compound	RI	Area percentage [%]		
			100 bar	200 bar	300 bar
1.	Hexanoic acid	973	0.01 ± 0.00	0.02 ± 0.01	0.02 ± 0.00
2.	Limonene	1033	0.07 ± 0.00	0.04 ± 0.01	0.05 ± 0.01
3.	2-Acetylpyrrole	1062	0.04 ± 0.01	0.05 ± 0.01	0.06 ± 0.01
4.	Octan-1-ol	1073	0.01 ± 0.00	0.02 ± 0.01	0.03 ± 0.01

5.	<i>cis</i> -Linalool oxide	1076	0.02 ± 0.00	0.01 ± 0.01	0.03 ± 0.01
6.	Linalool	1100	0.01 ± 0.01	0.01 ± 0.01	0.01 ± 0.01
7.	Menthone	1158	0.01 ± 0.00	0.01 ± 0.01	-
8.	Benzoic acid	1163	0.12 ± 0.02	0.18 ± 0.02	0.15 ± 0.01
9.	Octanoic acid	1173	0.02 ± 0.01	0.05 ± 0.01	0.04 ± 0.01
10.	Menthol	1175	0.08 ± 0.01	0.06 ± 0.02	0.06 ± 0.01
11.	(<i>Z</i>)-Hex-3-enyl butanoate	1190	0.07 ± 0.00	0.06 ± 0.01	0.08 ± 0.01
12.	α -Terpineol	1191	0.03 ± 0.00	0.03 ± 0.01	0.04 ± 0.01
13.	Geraniol	1257	0.05 ± 0.00	0.04 ± 0.01	0.05 ± 0.00
14.	Linalyl acetate	1260	0.03 ± 0.00	0.03 ± 0.02	0.02 ± 0.00
15.	Nonanoic acid	1270	0.02 ± 0.00	0.03 ± 0.01	0.03 ± 0.00
16.	2,6-Dimethylocta-1,7-diene-3,6-diol* (Terpendiol II)		0.10 ± 0.01	0.10 ± 0.02	0.12 ± 0.02
17.	Anethole	1286	0.03 ± 0.00	0.03 ± 0.01	0.04 ± 0.01
18.	Perilla alcohol	1297	0.03 ± 0.01	0.04 ± 0.01	0.04 ± 0.01
19.	Carvacrol	1301	0.01 ± 0.00	0.01 ± 0.00	0.02 ± 0.00
20.	<i>p</i> -Mentha-1,8-diene-1,2-diol	1341	0.25 ± 0.03	0.21 ± 0.01	-
21.	Decanoic acid	1368	0.06 ± 0.01	0.07 ± 0.00	0.08 ± 0.01
22.	Vanillin	1395	0.02 ± 0.00	0.02 ± 0.01	0.03 ± 0.00
23.	<i>trans</i> -Caryophyllene	1419	0.06 ± 0.01	0.04 ± 0.01	0.05 ± 0.01
24.	Undecanoic acid	1466	0.01 ± 0.01	0.01 ± 0.01	0.02 ± 0.00
25.	α -Curcumene	1484	-	-	0.20 ± 0.12
26.	α -Zingiberene	1495	-	-	0.33 ± 0.23
27.	β -Bisabolene	1509	-	-	0.17 ± 0.12
28.	β -Sesquiphellandrene	1525	-	-	0.20 ± 0.12
29.	Dihydroactinidiolide	1526	0.06 ± 0.01	0.03 ± 0.01	-
30.	Dodecanoic acid	1566	0.51 ± 0.13	0.56 ± 0.03	0.86 ± 0.01
31.	Spathulenol	1576	0.08 ± 0.01	0.06 ± 0.01	0.08 ± 0.01
32.	Caryophyllene oxide	1582	0.15 ± 0.02	0.12 ± 0.02	0.13 ± 0.03
33.	Veridiflorol	1589	0.05 ± 0.02	0.04 ± 0.01	0.03 ± 0.00
34.	Hexadecane	1600	0.03 ± 0.01	0.05 ± 0.01	0.04 ± 0.01
35.	α -Cadinol	1654	0.05 ± 0.00	0.04 ± 0.00	-
36.	Heptadecane	1700	0.04 ± 0.02	0.04 ± 0.00	0.06 ± 0.01
37.	Tetradecanoic acid	1763	0.29 ± 0.05	0.32 ± 0.03	0.45 ± 0.04
38.	Nootkatone	1800	0.46 ± 0.03	0.36 ± 0.02	0.41 ± 0.10
39.	Hexahydrofarnesyl acetone	1846	0.08 ± 0.01	0.08 ± 0.01	0.10 ± 0.03
40.	Hexadecan-1-ol	1880	0.24 ± 0.22	0.39 ± 0.08	0.57 ± 0.15
41.	Methyl hexadecanoate	1928	0.25 ± 0.02	0.28 ± 0.02	0.35 ± 0.14
42.	(<i>E</i>)-Hexadec-9-enoic acid	1942	0.08 ± 0.00	0.08 ± 0.02	0.13 ± 0.12
43.	Hexadecanoic acid	1970	20.58 ± 1.35	15.22 ± 1.16	15.27 ± 0.81
44.	Bergaptene	2048	1.75 ± 0.09	1.85 ± 0.35	2.51 ± 0.25
45.	Oleyl alcohol	2060	1.22 ± 0.08	1.09 ± 0.34	1.84 ± 0.48

46.	Octadecan-1-ol	2086	0.52 ± 0.46	0.53 ± 0.53	1.30 ± 1.30
47.	Methyl linoleate	2098	0.82 ± 0.44	0.89 ± 0.03	1.70 ± 0.70
48.	Oleic acid	2104	1.13 ± 0.74	2.05 ± 0.14	3.74 ± 0.63
49.	Methyl octadecanoate (Methyl stearate)	2130	1.07 ± 0.85	2.24 ± 0.39	1.60 ± 0.24
50.	Osthole	2135	5.42 ± 0.61	4.53 ± 0.14	5.11 ± 0.48
51.	Linoleic acid	2143	41.47 ± 1.83	38.80 ± 5.53	31.11 ± 3.18
52.	Ethyl stearate	2201	0.77 ± 0.20	1.07 ± 0.20	1.78 ± 0.01
53.	7-Methoxy-8-(2- formyl-2- methylpropyl)coumarin*	2206	1.00 ± 0.22	1.27 ± 0.27	2.31 ± 0.05
54.	7-Methoxy-8-(2-oxo-3- methylbutyl)coumarin*	2234	14.82 ± 2.13	12.65 ± 0.24	15.45 ± 2.99
55.	Tricosane	2300	0.34 ± 0.11	0.52 ± 0.20	1.02 ± 0.16
56.	Tetradecane	2400	0.35 ± 0.24	0.62 ± 0.26	0.23 ± 0.07

* Tentatively identified based only on MS data.

249

250 The supercritical OPD extracts obtained contain a wide range of compounds including mainly
251 fatty acids and their esters, terpenes, coumarins and their derivatives. Out of a total of 56
252 phytochemicals detected, 11 are fatty acids, of which linoleic (31.11-41.47%) and
253 hexadecanoic (15.22-20.58%) were the most common in all extracts. Apart from being an
254 important source of energy, each of these acids possess other activities. Linoleic acid is an
255 essential acid, and its consumption is of great importance for the human body. It can be
256 converted to arachidonic acid, which further serves as a precursor in the synthesis of a group
257 of hormones called prostaglandins, which have significant function in muscle contractions
258 and are also important due to their anti-inflammatory properties (Özcan et al., 2013).
259 Arachidonic and linoleic acid are omega-6 fatty acids, which have been shown to have
260 protective properties against cancer (Rajasekaran, 2017). Various clinical tests have proven
261 the local application of linoleic acid, as well as its polyunsaturated derivatives to reduce the
262 effects of transepidermal water loss, and also to achieve a soothing effect on the skin
263 (Ghafoor et al., 2017); this data could be of importance in the potential application of
264 supercritical OPD extracts in skin cosmetic preparation. Palmitic (hexadecanoic) acid as
265 saturated fatty acid present in the extracts obtained has been also shown to possess a wide

266 range of pharmacological activities, such as anti-inflammatory, antiviral, analgesic and
267 regulatory activity of lipid metabolism (Mayneris-Perxachs et al., 2014; Librán-Pérez et al.,
268 2019).

269 A study conducted by Jokić et al. (2020) showed the presence of fatty acids such as linoleic
270 and hexadecanoic acid in Sc-CO₂ extracts of orange peel. The abundance of fatty acids in
271 their study, at 300 bar and 40 °C was 4.8% for hexadecanoic and 9.2% for linoleic acid. Also,
272 the presence of fatty acids in the petrol ether extract of the orange peel after derivatization in
273 their methyl esters (Islam et al., 2012), as well as in the hexane extract of orange peel without
274 derivatization (Esquivel-Ferriño et al., 2014) has been reported.

275 Coumarins were identified as the second most represented group of compounds in the
276 supercritical OPD extracts, and these were: osthol (4.53-5.42%), bergapten (1.75-2.51%), 7-
277 methoxy-8-(2-formyl-2-methylpropyl)-coumarin (1.00-2.31%) and 7-methoxy-8-(2-oxo-3-
278 methylbutyl) coumarin (12.65-15.45%). Due to its various functions, this group of
279 compounds is very attractive. Namely, coumarins have a wide range of different biological
280 and pharmacological effects, such as anti-inflammatory, antiviral, antibacterial, antioxidant,
281 cyclooxygenase and lipoxygenase inhibition, antithrombotic, xanthine oxidase inhibition,
282 anti-Alzheimer's disease (AD), anticonvulsant, antidiabetic, as well as antitumor effects
283 (Annunziata et al., 2020). Thanks to their fungicidal and antioxidant effects, they are used as
284 additives in the cosmetics and food industry (Mark et al., 2019), and thanks to their aromatic
285 fragrance, their use in perfumes production is also significant (Matos et al., 2015). The
286 coumarin derivative identified in the highest amount was 7-methoxy-8-(2-oxo-3-
287 methylbutyl)coumarin (isomeranzin), which is found in the literature as one of the
288 constituents of citrus peel (Gyawali et al., 2012). However, the literature data on the
289 biological activity of the most dominant coumarin in the obtained supercritical OPD extracts
290 is rather limited, unlike data on others coumarins present. Osthol (7-methoxy-8-(3-methyl-2-

291 butenyl)coumarin), second dominant coumarin in the extracts obtained, is a natural coumarin
292 that exhibits anti-inflammatory, anticancer, neuroprotective, immunomodulatory properties,
293 as well as hepatitis suppressants (Zhang et al., 2015). Several studies have shown that this
294 compound enhances antitumor immune responses (Liu et al., 2015; Zhang et al., 2015) and
295 reduces the development of hepatocellular carcinoma (Zhang et al., 2012). During Sc-CO₂
296 extraction of bitter orange peel using ethanol as a co-solvent, Trabelsi et al. (2016) found the
297 presence of osthol as the main compound (47%). Also, according to the research of Jerković
298 et al. (2015), the presence of osthol in Sc-CO₂ extracts of orange peel from the Dubrovnik
299 region was detected (up to 1.1%). Coumarin bergapten or 5-methoxypsoralen, identified in
300 supercritical OPD extracts is the lower concentration up to 2,51%, is a furocoumarin
301 derivative and is mainly found in bergamot EO, but can also be isolated from other citrus EOs
302 as well as grapefruit juice (Sicari et al., 2018). According to Jerković et al. (2015) in the
303 extracts of the peel of different types of oranges from the Dubrovnik region obtained by Sc-
304 CO₂ extraction at 40 °C and 10 MPa, the presence of bergapten (up to 1.4%) was found too.

305 **3.2. Ultrasound-assisted extraction of OPD**

306 In the second part of this study, materials left after Sc-CO₂ extraction (SFE-100, SFE-200 and
307 SFE-300) were subjected to the UAE in order to isolate the polar constituents. The control
308 was performed using raw OPD (the material which was not subjected to the previous Sc-CO₂
309 step). By varying the extraction amplitude (20, 60 and 100%) from each processed material
310 three different OPD liquid extracts were obtained. Thus, totally 12 extracts were prepared and
311 further chemically analysed.

312 UAE is based on the mechanism of acoustic cavitation, where due to the implosion of
313 cavitation bubbles on the surface of plant material, damage or erosion occurs, which allows
314 easier contact with the solvent and the increased extraction yield (Petigny et al., 2013). It has

315 been proven that the UAE process is influenced by various parameters, of which special
316 emphasis is placed on the solvent, ultrasonic power, time, and temperature of the extraction.

317 The solvent stands out as a dominant parameter generally in the extraction processes, which,
318 regardless of the extraction technique, has a very significant impact (Tomšik et al., 2016) on
319 the process efficiency and product quality. Due to its high affinity for the phenols, ethanol
320 solution is considered the first-choice solvent for the extraction of phenolic compounds from
321 fruit and vegetable matrices and wastes (Ramić et al., 2015). As study conducted by Lapornik
322 et al. (2005) showed, the extraction efficiency is significantly reduced if pure ethanol is used
323 as the solvent because phenols (especially flavonoids with a sugar component) are hydrophilic
324 due to the number of hydroxyl groups, and thus show greater solubility in ethanol solutions.

325 According to Shehata et al. (2021), investigation of the effect of ethanol/water ratio (30 to
326 80%) on the polyphenol extraction from orange peel shows the total phenolic content
327 increases with the ethanol concentration up to 50%, emphasising that this concentration is the
328 optimal for maximum extraction of polyphenols from the orange peel. Besides, the
329 accessibility, origin from a renewable source, as well as categorisation as a GRAS solvent
330 (Rodrigues et al., 2015) are some of the additional reasons why ethanol solution is a suitable
331 solvent to be applied in the “green” process of OPD utilisation.

332 Based on all the above, 50% ethanol water solution was chosen as the solvent in this study,
333 while the influence of temperature and time was investigated. Since the UAE probe was used,
334 in addition to the above parameters, the analysis of power and energy consumption was also
335 considered.

336 Based on Figure 1A, the highest TPC was achieved in the liquid extract obtained from SFE-
337 100 material processed by UAE at an amplitude of 100% (24.43 ± 0.01 mg GAE/g dw). An
338 increase in TPC content in the liquid extracts obtained from SFE-100 can be clearly seen with

339 increasing amplitude, as well as a decrease in the value in the liquid extracts obtained from
340 other materials, SFE-200 and SFE-300. TPC in the liquid extracts obtained from the untreated
341 material (OPD not exposed to Sc-CO₂) increases with the increasing amplitude, with the
342 highest values reached at the highest amplitude, 22.94 ± 0.05 (mg GAE/g dw). If we compare
343 the quality of liquid extracts obtained from SFE-100, SFE-200 and SFE-300, with extracts
344 obtained from raw OPD untreated material, it can be noticed that higher concentration of
345 TPC, approximately up to around 6%, can be achieved if OPD was processed in the previous
346 step by Sc-CO₂ at 100 bar. Namely, the application of Sc-CO₂ extraction enabled the isolation
347 of low-polarity constituents, and the obtained degreased material without traces of toxic
348 organic solvents was used for further "cleaner and safer" processing, and at the same time, the
349 increased destruction of the material walls enabled the "easier" extraction of phenolic
350 constituents found in deeper layers . This is consistent with a study conducted by Rodríguez-
351 Rojo et al. (2012) where a positive effect of treatment with supercritical carbon dioxide on the
352 further isolation of phenolic constituents was observed.

353 The application of Sc-CO₂ prior to UAE was not beneficial in the case of flavonoid extraction,
354 as at all parameters applied the UAE of raw untreated OPD gave the better results. According
355 to the obtained results, in the case of untreated raw OPD material, there is a slight increase in
356 the liquid extracts TFC with increasing amplitude, reaching the maximum of 6.44 ± 0.01 (mg
357 CE/g dw) at the highest amplitude applied, what is the case if raw OPD material is processed.
358 Aside from this, it has been noticed that if the pretreated material is applied in this process, an
359 increase of amplitude in UAE will be beneficial, meaning the content of flavonoids in the
360 liquid OPD extracts produced will be increased in all cases (Figure 1B).

361 There are several studies in the literature which were focused on the application of UAE for
362 the isolation of polyphenolic constituents from the orange peel. Razola-Diaz et al. (2021)
363 determined TPC for orange peel using a sonotrode and the values obtained ranged between

364 8.7 and 29.7 (mg GAE/g dw). The highest value was achieved under ethanol/water (50:50,
365 v/v), for 25 min extraction, using 100% of amplitude and 100% pulse, while the lowest value
366 corresponds to application of 100% ethanol as extraction solvent, 25 min extraction, 20%
367 amplitude and 50% pulse. As the similar extraction procedure was applied, the difference in
368 TPC in the study of Razola-Diaz et al. (2021) and presented study most dominantly arise from
369 the difference in the quality of the starting raw material. According to Sandhu et al. (2021)
370 TPC of orange peel extract was 258.67 ± 1.14 (mg GAE/100 g), while for pulp it was 735.54
371 ± 1.83 (mg GAE/100 g) which is significantly less compared to the results of present study.

372 As already mentioned, temperature and time are important parameters of the UAE process. As
373 chemical changes in the extract can occur at elevated temperatures, as well as the degradation
374 of the target compounds, the process is set-up in such a way to allow the increase of the
375 process temperature up to maximal 50 °C. Therefore, the extraction time was dependable on
376 the temperature, while the temperature was dependable on the applied amplitudes. All three
377 were monitored. Figure 2 shows the time dependence of the temperature in the case of SFE-
378 100 material extraction, as a representative of the UAE of materials previously processed by
379 Sc-CO₂, while Figure 3 is showing the time change in the case of raw OPD extraction. As it
380 was expected, the decrease in the extraction time with increasing amplitude causes that at
381 higher amplitudes it takes a shorter time to reach a defined maximum process temperature.
382 Therefore, at amplitude of 20%, the extraction times were 20.5, 21 and 22 minutes for SFE-
383 100, SFE-200 and SFE-300, respectively, while at amplitudes of 60% and 100%, the time for
384 the tested samples was uniform, 5 and 3 minutes, respectively. In the case of the raw OPD
385 extraction the maximum temperature is reached somewhat faster, by 18.5, 4 and 2.5 minutes
386 at amplitudes of 20, 60 and 100%, respectively.

387 During the UAE, the energy consumption was also monitored (Figure 4). The increase in the
388 energy consumption over the time was observed, which would mean that changed process

389 parameters affect the final energy consumption. This needs to be considered too in order to
 390 select the most efficient process in terms of extract quality and energy consumption at the
 391 same time. This is especially important if the process results in the similar content of targeted
 392 bioactive compounds, such as in the case of UAE of TPC or TFC. In those cases, it is
 393 reasonable to select the process which saves energy.

394 The lowest energy consumption (6.566 W/h) was observed in the processing of SFE-100
 395 material at an amplitude of 60% in 5 min extraction, while the highest (10.115 W/h) was
 396 observed in processing of the SFE-300 at an amplitude of 20% in 22 minutes.

397 Table 2. UAE performance review.

Type of extracted material	Amplitude [%]	Time [min]	Energy [W/h]	TPC [mg GAE/g dw]	TFC [mg CE/g dw]
SFE-100	20	20.5	0.23 - 9.699	22.67 ± 0.04	5.82 ± 0.01
	60	5	0.75 - 6.566	24.41 ± 0.02	5.99 ± 0.01
	100	3	1.24 - 7.066	24.43 ± 0.01	6.2 ± 0.02
SFE-200	20	21	0.23 - 9.980	23.77 ± 0.04	5.83 ± 0.01
	60	5	0.72 - 6.818	23.25 ± 0.03	5.9 ± 0.01
	100	3	1.23 - 7.080	22.63 ± 0.02	6.17 ± 0.00
SFE-300	20	22	0.23 - 10.115	23.84 ± 0.01	5.81 ± 0.01
	60	5	0.73 - 7.022	22.97 ± 0.07	5.83 ± 0.01
	100	3	1.2 - 6.851	22.42 ± 0.06	6.09 ± 0.01
Raw OPD	20	18.5	0.31 - 9.348	21.31 ± 0.06	6.41 ± 0.01
	60	4	0.74 - 5.686	22.91 ± 0.05	6.42 ± 0.00
	100	2.5	1.26 - 6.1	22.94 ± 0.05	6.44 ± 0.01

398 From Table 2, if we want to draw a general conclusion based on all the results, the processes
 399 of material SFE-100 at an amplitude of 60% could be considered as optimal, as the TPC and
 400 TFC reached almost maximal value, while energy consumption is the lowest compared to all
 401 other cases of processing of material pretreated by supercritical process. Besides, the time is
 402 significantly saved as it is approximately 4 times lower than extraction time at amplitude
 403 20%, while it is just 2 minutes higher than extraction at amplitude 100%. Also, it is noticeable

404 that in all samples, during extractions with the longest duration, i.e. at an amplitude of 20%,
 405 the highest energy consumption occurs.

406 3.3. HPLC chromatographic profiling of liquid OPD extracts

407 HPLC analysis liquid OPD extracts obtained in UAE confirmed the presence of bioactive
 408 compounds, namely hesperidin, naringin, narirutin and rutin. According to the literature data
 409 the two most dominant flavonoids, in fresh and dried orange by-products, were hesperidin and
 410 narirutin (Razola-Díaz et al., 2021). Londoño-Londoño et al. (2010) studied the application of
 411 UAE in the extraction of polyphenols from the citrus peel. According to their study, orange
 412 peel was the most complex source of these bioactive compounds as it contained hesperidin,
 413 neohesperidin, diosmin, nobiletin and tangerine and. In another study, M'hiri et al. (2017)
 414 identified 10 phenolic compounds in ethanolic extracts of Maltese orange peel, namely
 415 flavanones (eriocitrin, narirutin, naringin, hesperidin, neohesperidin, didimine) and
 416 polymethoxylated flavones (sinensetin, hexamethoxyflavone, tangeretin, nobiletin). The
 417 extracts were obtained by various methods, and one of the ones used was UAE with the use of
 418 a sonicator. Toledo-Guillen et al. (2010) identified hesperidin, narirutin, sinensetin, nobiletin,
 419 tetramethylscutellarein and tangeretin in orange peel extracts.

420 Table 3. Components detected by HPLC in OPD extracts.

Samples	Amplitude [%]	Hesperidin [µg/ml]	Narirutin [µg/ml]	Naringin [µg/ml]	Rutin [µg/ml]
SFE-100	100	860.08 ± 6.31	17.08 ± 0.26	804.04 ± 9.28	75.10 ± 27.56
	60	865 ± .35	17.23 ± 0.08	809.05 ± 5.10	48.37 ± 0.03
	20	848 ± 6.50	17.10 ± 0.13	794.13 ± 2.83	48.31 ± 0.55
SFE-200	100	863.6 ± 2.55	17.31 ± 0.19	801.77 ± 0.38	48.70 ± 0.42
	60	857.13 ± 1.73	17.20 ± 0.19	795.89 ± 3.99	47.92 ± 0.04
	20	884.64 ± 21.59	16.70 ± 0.51	771.45 ± 28.66	47.53 ± 0.67
SFE-300	100	849.13 ± 12.23	16.81 ± 0.06	785.56 ± 12.64	104.40 ± 0.18
	60	878.30 ± 33.60	17.34 ± 0.35	814.18 ± 32.64	48.10 ± 0.11

	20	852.57 ± 13.82	16.92 ± 0.10	781.03 ± 4.29	47.58 ± 0.57
	100	900.24 ± 0.21	18.16 ± 0.12	830.39 ± 0.62	100.44 ± 0.58
Initial OPD	60	865.62 ± 0.60	17.61 ± 0.43	797.22 ± 0.42	50.66 ± 0.93
	20	891.13 ± 0.89	17.85 ± 0.31	824.09 ± 0.64	100.06 ± 0.24

421

422 As already mentioned, the most common flavonoid in the orange peel is hesperidin. In this

423 research, this statement was confirmed even though the study investigated the orange peel

424 dust which is actually the orange peel waste product. Based on Table 3, the content of

425 hesperidin is the highest compared to the other identified components. The second dominant

426 flavonoid in liquid OPD extracts was naringin, present in just some lower concentration in

427 comparison to hesperidin. According to the literature using an ultrasound sonifier, Khan et al.

428 (2010) isolated hesperidin and identified it as the main compound of orange by-products

429 present in the amount of 205.2 mg/100 g fresh weight. Giannuzzo et al. (2003) and Taktak et

430 al. (2018) conducted studies on extraction methods, which showed the effect of processing

431 variables on naringin release. Comparing the yields obtained after UAE and solvent extraction

432 (SE) for 60 min extraction, Wang et al. (2008) found out that the amounts of naringin and

433 hesperidin obtained in UAE (70.3 and 205.2 mg/100 g fresh weight, respectively) were

434 significantly higher than those obtained by SE (50.9 and 144,7 mg/100 g fresh weight,

435 respectively). Authors of the same study stated that no evidence was found that flavanone

436 degradation occurred under sonication, and based on the yield, it was confirmed that the UAE

437 was significantly more efficient. Same has been noticed in the study of Khan et al. (2010)

438 where results of the Valencia orange peel variety extraction were presented. This is in line

439 with the fact that the UAE has the potential to extract natural compounds with higher yields

440 than conventional techniques. The concentration of hesperidin, in the liquid OPD extracts

441 obtained by UAE from materials pretreated by Sc-CO₂, ranges from 848 ± 6.50 to 884.64 ±

442 21.59 (µg/ml). If the process of OPD utilisation is set without supercritical pretreatment, then

443 liquid OPD extracts with some higher concentration of hesperidin can be obtained. But, in this
444 case the concentration of hesperidin is higher up to 1,8%, and what needs to be kept in mind
445 is that the non-polar fraction is lost as it is not prior isolated by a supercritical process.
446 Glycosylated flavonoid naringin, known for its antioxidant activities (Nakao et al., 2011)
447 ranged in the liquid OPD extracts obtained from previously pretreated materials, between
448 771.45 ± 28.66 and 814.18 ± 32.64 ($\mu\text{g/ml}$), with the highest concentration measured in the
449 extract obtained from SFE-300 sample by application of 60% amplitude. Similar as in the
450 case of hesperidin, its concentration can be increased in the liquid extracts if the untreated
451 OPD is applied at the amplitude of 100%, but again, this means that non-polar fraction will be
452 lost as isolation in the supercritical phase will not be applied.

453 Compounds detected in the lower concentration in the liquid OPD extracts are narirutin and
454 rutin. The content of narirutin ranged between 16.70 ± 0.51 and 17.34 ± 0.35 ($\mu\text{g/ml}$) for
455 extracts obtained from samples previously processed by Sc-CO₂. The concentrations of
456 narirutin in these extracts were quite similar regardless to the material or amplitude applied.
457 Slightly higher results were determined in the liquid extract obtained from the previously
458 untreated OPD material, but again quite similar regardless of the amplitude applied. Rutin is a
459 glycoside of the flavonoid quercetin, which is characterised by a strong antioxidant effect. It
460 is found in many plant fruits, as well as in fruit peels (especially in citrus fruits: oranges,
461 grapefruit, lemon and lime) (Omoba et al., 2015). In the study of Omoba et al. (2015) routine
462 concentrations ranged between 18.6 and 17.93 mg/g for mature and immature peels,
463 respectively. In the present study, rutin was identified in the liquid OPD extracts (obtained
464 from material processed by Sc-CO₂) at a concentration of 47.53 ± 0.67 to 104.40 ± 0.18
465 ($\mu\text{g/ml}$). The highest concentration was determined in SFE-300 extract using UAE at the
466 amplitude of 100%.

467 **3.4. Predicted pharmacological potential of extracts**

468 As established previously, the extracted compounds have a wide range of important activities,
469 with the mechanism of action not fully established for the most of the compounds. In this
470 study, we focussed on the two most abundant non-fatty acid molecules found in the extracts
471 obtained using Sc-CO₂ extraction, isomerazin and osthole. These were chosen for further *in*
472 *silico* studies that include protein target prediction and evaluation of potential interaction with
473 putative targets. Linoleic and hexadecenoic acids, most abundant fatty-acids, were considered
474 as the candidates for synergistic action on a selected target. Besides, all four constituents
475 detected in the liquid OPD extracts obtained by UAE (hesperidin, naringin, narirutin and
476 rutin) were evaluated too.

477 The Pharmmapper results indicated that the top scoring targets for isomeranzin and osthole do
478 not have specified indications (Table 4), leading the choice of liver carboxylesterase 1 (CES1)
479 as a potential target for coumarin analogues. The indications for this protein listed by
480 Pharmmapper include a range of diseases arteriosclerosis, hypercholesterolemia,
481 hyperlipidaemia, cardiovascular and cerebrovascular diseases, various cancers and multiple
482 myeloma, Alzheimer's disease, dementia and osteoporosis. Interestingly, three out of four
483 main components identified in the liquid OPD extracts obtained by UAE have a potential to
484 interact with the same protein, albeit with lower certainty as indicated by lower z-scores.

485 Previous studies have shown that citrus peel can have beneficial preventative effects in
486 atherosclerosis (Feng et al., 2020) and cancer, suggesting that interactions of its components
487 with the CES1 could be further explored.

488 Table 4. Potential top scoring targets of selected components of OPD extracts predicted using
489 Pharmmapper. Detailed information is included for liver carboxylesterase 1, a putative target
490 of isomerazin, with defined indications.

Compound	Top scoring target		Liver carboxylesterase 1		
	Name	Indication	Rank	Normalised fit	Z-score
Isomerazin	Stromelysin-1	None	2	0.99	1.26
Osthole	ATP synthase C chain	None	12	0.98	1.13
Linoleic acid	Steryl-sulfatase	Cognitive disorder; Cancer	40	0.87	1.19
Hexadecanoic acid	NitFhit	None	179	0.82	0.70
Hesperidin	Xylose isomerase	Scurvy	-	-	-
Naringin	Arylesterase	None	111	0.92	0.01
Narirutin	Xylose isomerase	Scurvy	113	0.93	-0.08
Rutin	Lysozyme	Myasthenic syndrome	198	0.87	-0.46

491

492 Table 5. Molecular properties (logP and solubility) and drug likeness of selected compounds
 493 predicted using DataWarrior software. The results of the molecular docking of these small
 494 molecules into the binding pocket of liver carboxylesterase 1 are shown as binding affinities
 495 of top binding poses calculated using Vina software.

Compound	clogP	clogS	Druglikeness	Binding affinity (kcal/mol)
Isomerazin	2.26	-3.2	-5.64	-8.1
Osthole	3.44	-3.3	-3.29	-7.7
Linoleic acid	6.47	-4.3	-25.56	-6.2
Hexadecanoic acid	6.06	-4.2	-25.22	-5.5
Hesperidin	-0.81	-2.7	2.04	-9.5
Naringin	-0.74	-2.7	0.64	-9.7
Narirutin	-0.74	-2.7	1.89	-10.0
Rutin	-1.26	-2.4	1.93	-8.5

496

497 Molecular docking simulations have shown that all molecules can be accommodated into the
 498 CES1 active site with different binding affinities (Table 5). Isomerazin and osthole bind with
 499 similar binding scores, and they form favourable interactions in two different parts of the
 500 binding site that are promiscuous. However, both molecules interact with a residue of
 501 catalytic triad residues (S1221–E354–H468) that is located at the base of the active gorge.

502 These interactions have a potential to prevent generation of the Ser221 oxygen nucleophile
503 and disrupt the action of the enzyme (Briand et al., 2019).

504 Similar types of interaction can be formed by other docked molecules (Figures 5C, 5D and 6),
505 except the naringin which interacts with another residue of the catalytic triad, H1468.

506 Although the four compounds from liquid OPD extract obtained by UAE have better binding
507 affinities, they have lower predicted gastrointestinal absorption and may have lower inhibitory
508 potential than isomerazin and osthole due to potentially lower blood concentrations. However,
509 they can contribute additively to the action of the extract against CES1. Overall, these small
510 molecules from the extracts can act as non-specific inhibitors of CES1 and therefore could
511 modulate its function resulting in multiple beneficial effects. However, it should be also
512 considered that these molecules can also affect the function of other proteins and that warrants
513 further investigation.

514 **4. Conclusions**

515 Based on the results of the study, it can be concluded that the OPD is a rich source of
516 bioactive compounds and therefore should be further utilised for more valuable products-
517 extracts production. Fatty acids (linoleic, hexadecane and oleic), 7-methoxy-8-(2-oxo-3-
518 methylbutyl) coumarin and osthole were present as dominant compounds in Sc-CO₂ extracts,
519 while in UAE extracts hesperidin, naringin, narirutin and rutin were the most abundant. In the
520 utilisation pathway it is meaningful to combine two green extraction techniques for isolation
521 of first non-polar constituents (Sc-CO₂ extraction), and then, in the second phase, to isolate
522 the polar one using UAE and ethanol solution as the extraction solvent. Although the general
523 results of the UAE are showing that liquid OPD extracts obtained by UAE alone, without
524 previous supercritical extraction, contained slightly higher concentration of the dominant
525 polar bioactive compounds, this difference is not of the significant level to favour the

526 application of UAE without previous supercritical extraction step. Depending on the selection
527 of targeted-priority compounds, the optimal conditions could be viewed from two different
528 perspectives. However, if both polar and non-polar compounds are equally important, and if
529 the goal of final producer is production of two different extracts-fitopreparation from the
530 orange peel herbal dust, Sc-CO₂ extraction at 200 bar and then ultrasound-assisted extraction
531 at an amplitude of 60% could be considered as the optimal conditions. In this way, a sufficient
532 amount of non-polar compounds would be isolated, and on the other hand, second extract
533 with the high concentration of both, TPC and TFC, as well as the dominant polar compounds
534 will be produced, with significant energy savings.

535 According to the *in silico* evaluation the obtained extracts, due to the bioactive constituents
536 present, are showing a wide range of important activities. Results of the investigation are
537 indicating the potential application toward atherosclerosis prevention.

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834 **Figure captions**

835 Figure 1. Influence of UAE amplitudes on A) the TPC and B) TFC of raw OPD, and SFE-
836 100, SFE-200, and SFE-300 samples.

837 Figure 2. Dependence of the process time on the process temperature in the case of SFE-100
838 material extraction.

839 Figure 3. Dependence of the process time on the process temperature in the case of raw OPD
840 extraction.

841 Figure 4. Dependence of energy consumption presented for the case of on the UAE of SFE-
842 300 material.

843 Figure 5. Top binding poses of components from supercritical OPD extracts docked into liver
844 carboxylesterase 1 binding site, A) isomerazin, B) osthole, C) linoleic acid and D)
845 hexadecanoic acid. The amino acid residues of the protein are shown in a thin line
846 representation, while the small molecules are shown as thick cyan bond in 3D plots, while the
847 amino acid residues are shown as circles coloured according the type of the interaction
848 involved with small molecules (thick stick representation (light green – van der Waals
849 interaction, dark green – conventional hydrogen bond, pink – interaction involving alkyl
850 groups, purple – pi-sigma interaction, dark pink – amide -pi stacked interaction).

851 Figure 6. Top binding poses of components from liquid OPD extracts obtained by UAE
852 docked into liver carboxylesterase 1 binding site, A) hesperidin, B) naringin, C) narirutin and
853 D) rutin. The amino acid residues of the protein are shown in a thin line representation, while
854 the small molecules are shown as thick cyan bond in 3D plots, while the amino acid residues
855 are shown as circles coloured according the type of the interaction involved with small
856 molecules (thick stick representation (light green – van der Waals interaction, dark green –

857 conventional hydrogen bond, pink – interaction involving alkyl groups, purple – pi-sigma
858 interaction, dark pink – amide -pi stacked interaction).